AMENDMENT TO THE CLAIMS:

The following claim set replaces all prior versions, and listings, of claims in the application:

- 1. (original) Process for purification of a compound comprising an activated carbon treatment using a filter unit containing activated carbon immobilized in a matrix, the treatment comprising:
 - a) passing a suitable volume of a feed containing the compound over a first series of n connected filter units operating in series to obtain an effluent, wherein n is at least two, said filter units having been assigned a position number 1 to n in the series and position number 1 being the first supplied with the feed.
 - b) disconnecting a filter unit from the first series of filter units at any position number between. 1 to n-1 after passing the suitable volume of feed, and connecting a fresh filter unit at any position that has a higher number than the position number of the disconnected filter unit, resulting in a next series of filter units,
 - c) passing a next suitable volume of feed containing the compound over the next series of filter units to obtain a next effluent,
 - d) optionally combining the effluents obtained in a and c, and
 - e) recovering the compound from the effluent.
- 2. (original) The process according to claim 1, wherein the filter unit is disconnected at position number between 1 to n-1 and wherein the fresh filter unit is connected at position number n+1.
- 3. (original) The process according to claim 1, wherein the filter unit is disconnected at position number 1 and wherein the fresh filter unit is connected at position number n+1.

- 4. (previously presented) The process according to claim 1 wherein the number n of connected filter units operating in series is 2 to 10.
- 5. (previously presented) The process according to claim 1, wherein the treatment is operated in batch, semi-continuous or continuous mode.
- 6. (previously presented) The process according to claim 1, wherein the flow rate of the feed is 0.05 to 400 L/min, preferably 20 to 100 L/min, more preferably 30 to 40 L/min.
- 7. (previously presented) The process according to claim 1 wherein the activated carbon immobilized in a matrix is in the form of a membrane sheet.
- 8. (original) The process according to claim 7, wherein the flux over the membrane sheet is 1 to 50 L/m2/min., preferably 1.5 to 20 L/m2/min., more preferably 1.5 to 10 L/m2/min.
- 9. (previously presented) The process according to claim 1, wherein the residence time of the feed containing the compound in a single filter unit is at least 15 seconds and maximal 60 minutes.
- 10. (previously presented) The process according to claim 1, wherein the process is operated at a temperature between minus °C to 40°C.
- 11. (previously presented) The process according to claim 1, wherein at least one disconnected filter unit is regenerated *in situ* by rinsing with a solvent.
- 12. (previously presented) The process according to claim 1, wherein the compound is an unstable compound.
- 13. (currently amended) The process according to claim 12, wherein the compound is a secondary metabolite or a protein.

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- 14. (original) The process according to claim 13, wherein the secondary metabolite is selected from the group consisting of an antibiotic, a vitamin, a carotenoid or a PUFA.
- 15. (currently amended) The process according to claim 12, wherein the compound is obtained by fermentation using a microorganism.
- 16. (original) The process according to claim 14, wherein the microorganism is a *Streptomyces* species.
- 17. (original) The process according to claim 15, wherein the *Streptomyces* species is selected from the group consisting of *S. clavuligerus*, *S. coelicolor*, *S. griseus*, *S. venezuela*, *S. jumonjinensis*, *S. katsurahamanus* or *S. aureofaciens*.
- 18. (currently amended) The process according to claim 14, wherein the compound is selected from the group consisting of clavulanic acid, streptomycin, chloramphenicol, tetracycline or p3-carotene β -carotene.
- 19. (previously presented) The process according to claim 1, further comprising the step of converting the compound into a pharmaceutical acceptable salt or food grade product.